THERMOPTIM®

Spark ignition engine example

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Reciprocating internal combustion engine cycle

Let us study a reciprocating internal combustion engine whose corresponding theoretical cycle takes into account a multi-step combustion process. We shall in this example analyse the spark ignition engine.

After a 0.9 isentropic efficiency compression, start a combustion that unfolds in three phases:

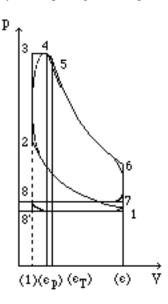
- the first one, at constant volume, allows the pressure to reach its maximum in the cycle,

- the second one, at constant pressure, leads to the maximum temperature

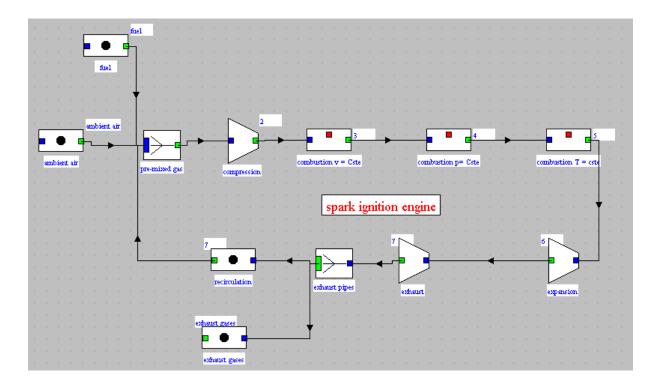
- the end of the combustion takes place at constant temperature.

- gases are then expanded to the bottom dead center (bdc), with an expansion isentropic efficiency equal to 0.95

Due to the clearance volume, 3.3% of the burnt gas mass are assumed to recirculate.



 ϵ compression ratio ϵ_p isobaric cutoff ratio ϵ_T isothermal cutoff ratio



This cycle corresponds to the following diagram which can easily be built in the graphical editor:

Solution of the problem

The approach is very close to that of the diesel engine, to which the reader should refer, the main difference coming from that the intake mass initially comprises the fuel, and that therefore ulterior combustion is made without other fuel addition. In these conditions, the mixer is comprised of three fluids: the recycled gases, the ambient air, and the fuel. After some iterations, one gets, for example, the project below.

node pre-mixed	gas ty	ype mixe	r		< >	Save
main process	display	m global	1.067		Suppress	Close
compression		h global	22.06		Calculate	
		T global	45.89			
process name	m abs	Τ ((°C)	Н	add a branct	
ambient air	0.967	15		-9.87	auu a manci	1
recirculation	0.033	852.56		984.99		
fuel	0.067	30		8.57	delete a brand	h

The intake fuel mix (close to the stoichiometric mix) has for these conditions the following composition (one keeps the same chemical formula for the fuel as in the diesel engine example):

component name	molar fraction	mass fraction
N2	0.7644739	0.7072499
Ar	0.008809558	0.01162292
02	0.1992529	0.2105633
CO2	0.002901183	0.004216664
H2O	0.003545039	0.002109145
со	0.001442814	0.00133467
H2	0.0005033247	0.00003350868
C7,2H13,42 `carb	0.01907133	0.06286994

The presence of CO and H2, in tiny quantities, comes from the recirculation of exhaust gases.

After the compression (volumetric ratio equal to 8, e.g. smaller than that of the diesel to avoid detonation), the constant volume combustion until 50 bar gives the following screen:

process C	combustion v = Cste type	combustion			<	>	Save
energy ty	purchased	set flow		links	Supr	vstem	Close
inlet point		flow	rate 1.067		open sys	-	
2	display	Delta_U	1,665.31			Calcula	te
T (°C)	391.19	w	0				
p (bar)	14.9959	ft	iel				
h (kJ/kg)	410.09	Ľ	CHa type	a	0		
quality	1			hf0	0		
outlet poir	nt	Ľ	dissociation	dissociat	ion degree	0.07	
3	display				g temp	1,500	
				combusti		0.97417	
T (°C)	1,872.45			chamber	efficiency	0.81	
p (bar) h (kJ/kg)	2,395.48				ksi	0.74	
quality	1	F	Calculate T		T (°C)	1,872.44	55987796
quanty	·		Set the fuel flo	w rate			
			set pressure		V	by the inle	t point
		Ľ	set volume			by the use	-
			set temperatu	re			

As it is clear, in this case, that the notion of air factor λ loses its meaning, this parameter is used to represent the burnt fraction of the reactants ξ . If $\xi < 1$, one considers that only a fraction x of the mix has reacted, and that (1- ξ) has not reacted. Combustion gases are then considered as a dual mix gas: there are the reaction products, including inert gases, and the fraction of the initial mix that has not reacted.

Here, one has adjusted ξ to obtain p = 50 bar.

The burnt gas composition, considering the dissociation, becomes:

component name	molar fraction	mass fraction
N2	0.7388013	0.7076713
Ar	0.008513715	0.01162985
02	0.05006601	0.05477908
CO2	0.09762823	0.1469139
H2O	0.09414534	0.05799332
со	0.004769617	0.004568156
H2	0.001283761	0.00008848855
C7,2H13,42 `carb	0.004792029	0.01635592

The combustion	continues at c	constant pressure	, until it reaches a	temperature of 2250 K:

process	combustion p=	Cste type	combusti	on				<	>	S	ave
energy ty	pe purchased		set flow	W		links		Suppi osed sy			lose erved
inlet point			fle	ow rate	1.067			en syst			aveu
3		display	Delta_U	1	56.31]		Calcul	ate	Ī
T (°C)	1,872.45		w	3	86.01			I]
p (bar)	50.0681			fuel							
h (kJ/kg)	2,395.48			🗹 CHa	type	а	0				
quality	1					hf0	0				
outlet poir	nt			🗹 disse	ociation	dissocia	ation deg	jree	0.08		
4		display				quenchi	ng temp		1,500		
L] L					combus	tion eff.		0.88733	3	
T (°C)	1,976.29					chambe	r efficie	ncy	0.81		
p (bar)	50.0681		,				ksi		0.26		
h (kJ/kg)	2,541.41			🗹 Calc	ulate T		Т (°	C)	1,976.2	87571358	
quality	1			🗌 Set t	he fuel fla	ow rate					
				🗹 set p	ressure						
				🗌 set v	olume				y the inl y the us		
				🗌 set t	emperatu	ire			y the us	CI	

The burnt gas composition becomes:

component name	molar fraction	mass fraction
N2	0.7365418	0.7101736
Ar	0.008487677	0.01167097
02	0.03693553	0.04067985
CO2	0.1011109	0.1531612
H2O	0.1006522	0.06241166
со	0.009916998	0.009560945
H2	0.002819611	0.0001956389
C7,2H13,42 `carb	0.003535256	0.01214618

rocess C	ombustion T	= cste type	combustion				>	Save
energy typ	purchase		set flow		links	Sup	press	Close
inlet point	Ľ		flow rate	1.067		Closed s	-	observe 🗌
4		display	Delta_U	318.36			Calculat	e
T (°C)	1,976.29		W	337.66				
p (bar)	50.0681		fuel					
h (kJ/kg)	2,541.41		CH	a type	а	0		
quality	1				hf0	0		
outlet poir	at		🖌 dis	sociation	dissocia	ation degree	0.1	
5	ĸ	display			quenchi	ng temp	1,500	
L	J				combus		0.74195	
T (°C)	1,976.29				chambe	r efficiency	0.81	
p (bar)	33.5954					ksi	0.8	
h (kJ/kg)	2,541.65		🗹 Cal	culate T		T (°C)	1,855.928	386
quality	1		🗌 Set	the fuel fl	ow rate			
			🗆 set	pressure		_		
			🗌 set	volume			by the inlet by the user	-
			🗹 set	temperati	ure		by the user	

Finally, the constant temperature combustion gives, with $\xi = 0.8$ that takes into account the presence of non burnt gases:

Exhaust gases contain some fuel and oxygen, as well as carbon monoxide and hydrogen.

component name	molar fraction	mass fraction
N2	0.7314482	0.7284202
Ar	0.00842898	0.01197083
02	0.007336021	0.00834501
CO2	0.08714399	0.1363388
H2O	0.1064837	0.06819569
со	0.04333837	0.04315434
H2	0.01511856	0.001083447
C7,2H13,42 `carb	0.0007021616	0.002491651

The expansion phase can be represented. It takes place between points 5 and 6, of similar composition. The volumetric expansion rate ρ_{56} is calculated. THERMOPTIM assumes that the volume v_6 at the bottom dead center (bdc) is known. If one calls V_i and m_i the total volume of the cylinder and the mass in the cylinder at point i, one has the following relationships:

 $\rho_{56} = V_6/V_5 = (m_6 v_6)/(m_5 v_5) = v_6/v_5$ since $m_6 = m_5$

Furthermore $\rho = V_6/V_2 = (m_6 v_6)/(m_2 v_2) = (m_5 v_6)/(m_2 v_2)$, and $\rho = V_1/V_2$

 $v_6 = \rho (m_2 v_2)/m_5 = v_1 m_1/m_5 = v_1 since m_1 = m_5$

The specific volume at the bdc is therefore equal to that of point 1. It therefore correspondingly has to be modified manually in order to take into account this phenomenon.

Finally, the indicated efficiency of the cycle is less than that of the diesel engine:

Ba	alance
efficiency	0.41662
seful energy	891.55
urchased energy	2,139.97

After correction with the thermal efficiency (0.81) and the sweeping cycle, it has a value of 33.7 %.

The project file is "gasoline.prj" and the diagram file "gasoline.dia".

It should be noted that the automatic recalculation cannot be fully automated here. The reason is that the combustion in the motor cylinder is represented as a sequence of three closed system combustions: first constant volume, second constant pressure and third constant temperature. This corresponds to very specific parameter settings which are not taken into account by the calculation process, as for instance the setting of ξ to get the right pressure or temperature or the update of v₆.

Viewing the point state values in the diagram editor

The results obtained may be displayed on the diagram (the values differ slightly from those shown above as the initial settings were not exactly the same):

